

Experimental evaluation of tube and tube heat exchanger for water-water and water-salt solution combination

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Abstract

Tube and Tube heat exchanger (TTHE) is designed with help of solidworks and simulation done with Ansys software. The TTHE is fabricated with stainless steel metal and it is prepared to compare the heat exchange between waterwater and water-salt solution. Experimental results show that the heat exchange rate in water-water combination (256.7) is comparatively higher than water – salt solution combination (91.78). Thermal conductivity, density and specific heat of solutions are considered in experimentation. It is observed that variation in flow rates are directly proportional to the inlet and outlet temperature of TTHE. It seems that turbulence allowance may affect flow rate of the solutions and it might have impact on heat exchange rate.

Keywords: Tube and Tube heat exchanger, Flow rate, Water-water combination, water-salt solution combination

1. Introduction

Heat exchanger is one of the important devices in heat transfer process in various fields like industries, construction sites, transports and others. The heat exchanger is found in large constructions to support cooling process such as fossil fuel power plant. The heat exchanger is a device which transfers the heat from hot medium to cold medium without mixing both the mediums since both mediums are generally separated with the solid wall. There are different types of heat exchanger that are used based on the application, e.g. Tube and Tube heat exchanger is used in chemical process like condensing the vapor to the liquid. To construct this type of heat exchanger, type of material should be selected wisely since it affects the overall heat transfer coefficient.

There are many studies and experimentation has been performed on the topic of Heat Exchanger which has been reviewed in research. Apu Roy, D.H.Das has conducted study on analysis of a shell and finned tube heat exchanger using CFD for waste heat Recovery applications in 2011. They found, the increasing of velocity the Heat transfer also increased. Also, Temperature increases along the fins tube and in case of shell the temperature is decreasing.

K.Sivakumar, K.Rajandid analysis of Heat Transfer and Effectiveness on Laminar Flow with Effect of different Flow Rates in 2014-15. They did experimental investigation of heat transfer and friction factor characteristics with different flow rates by means of CFD simulation. This work is conducted by the double pipe heat exchanger with opposite flow direction.

K. Sivakumar, Dr. K. Rajan, S. Murali, S. Prakash, V. Thanigaivel, T. Suryakumar conducted a Experimental Analysis Of Heat Transfer And Friction Factor For Counter Flow Heat Exchanger in 2015.

They studied heat transfer and effectiveness of the double pipe heat exchanger with two flow directions. One is parallel flow and counter flow direction. A commercial CFD package, Ansys fluent version are used for this study.

For this research, the small heat exchanger is constructed which I want to make practical in daily life such as for oil refineries and their chemical processes. Good design for the small Tube and Tube heat exchanger is selected. Good design referred to heat exchanger with least possible area & pressure drop to fulfill heat transfer requirement.

In this experimentation, Inner tube side hot water rejects heat to the outer shell side cold water. The properties of materials and its size are considered in design process. Heat exchanger is fabricated by using cutting, TIG welding and drilling. The experiment is performed for two combinations water-water and water-salt solution. Hot water is inside the tube and shell side fluid is normal water for first combination and salt solution for second combination. The experiment is performed under three different conditions where, i) Hot and cold water flow rate is manipulated for 7:1 concentration for salt water-water combination.

ii)By keeping tube side and shell side fluid flow rate constant.

iii)By varying salt water concentration.

2. Experimental analysis of heat exchanger

2.1Solidworks Model

Solid works is used for designed the TTHE. Below are some key figures of design.









Fig.2 Solidworks 3 D model

Fig.1 and fig.2 shows the heat exchanger 2-D and 3-D model as per specification.

2.2 Mathematical Formulation:

 $Q = A \times V$

Q = discharge (m^3/s) A= area (m^2) V = velocity (m/s)

 $Q_{\text{Rejected}} = m \times C_p \times \Delta T$

(2)

"Q_{Rejected}" = Heat Transfer m = mass flow rate

C_p= specific heat at constant volume ΔT = change in temperature

2.3 Project Layout





Fig. shows project layout contains two pumps, two flow control valves, heating chamber, heat exchanger, water tanks. Water is taken from water tank by first pump. Flow control valve mounted next to the pump to manipulate flow of fluid. Water is then pass through heating chamber by pneumatic pipes. This heated water is used as shell side fluid.

Similarly, room temperature water is taken from second water tank through second pump and this flow is controlled by second flow control valve. This water is used as shell side fluid for water-water combination. For water-salt solution combination shell side fluid is salt solution. Inlet and outlet temperatures of outer shell side and inner tube side fluid are measured and used for calculation purpose.

2.4Fabrication



The basic components of an Tube& Tube Heat Exchanger are:

- Heat Exchanger
- Two 2kw Heating Coils
- Heating Chamber
- **4 Digital Thermometers**
- 2 Pumps
- 2 Gate valves
- (1)^{arch} in Engin• pneumatic pipe

heat exchanger is fabricated by using cutting, bending, TIG welding and drilling.







Fig.4Fabrication work



Fig.5Experimental Setup

2.5 Calibration

For calibration of temperature measuring devices the laser thermometer was compared with thermocouple and the following readings were obtained-

- - for hot water : leaser thermometer reading is 68.8 degree and thermocouple reading is 69.1 degree.
- - for cold water + ice : leaser thermometer reading is 4.3 degree and thermocouple reading is 4.0 degree.
- - for room temperature water : leaser thermometer reading is 4.3 degree and thermocouple reading is 4.0 degree.
- - for room temperature: leaser thermometer reading is 37.2 degree and thermocouple reading is 37.0 degree.



Fig.6Comparing laser thermometer with thermocouple *2.6 Observation Table*

The observations obtained are as follows:

2.6.1 Observation for 7:1 concentration for salt waterwater combination:

Table 2.6.1 Observation table for 7:1 concentration for salt water-water combination

1.	01 1			m 1				
combi	Shel	l side		Tube side				
nation					-			
		Inlet	Outlet	Flow	Inlet	Outlet		
	Fl	wate	water	rate	water	water		
	0	r	temper	(lps)	temp	temper		
	w	temp	a <mark>ture(°</mark>	2	eratu	ature		
	ra	eratu	C)	D	re	(°C)		
	te	re(°C			(°C)			
	(lp)	ć	5				
	s)		Č	2				
Water	1/	27	30 0	171	86.8	76		
-	10		la Ia			-		
water	7	Λ						
Water	1/	29	31.5	148	82.5	78.7		
-salt	20							
soluti	2							
on		ii.						
Water	1/	28	31.2	175	88.9	79		
	.110	n						
water ^e	0							
Water	-1/	30	32.8	151	85.5	81.2		
-salt	20			-		-		
soluti	5							
on	-							
Water	1/	29	32.1	168	85.6	74.1		
-	10							
water	6							
Water	1/	30	33	145	81.2	76.6		
-salt	, 19							
soluti	8							
on								

2.6.2 By keeping tube side and shell side fluid flow rate constant:

Table 2.6.2 Observation table for By keeping tube side and shell side fluid flow rate constant



combi	Shel	l side		Tube side					
nation									
	Fl o w ra te (lp s)	Inlet wate r temp eratu re(°C)	Outlet water temper ature(° C)	Flow rate (lps)	Inlet water temp eratu re (°C)	Outlet water temper ature (°C)			
Water - water	1/ 18 0	28	31.6	1/1 90	83.4	70			
Water -salt soluti on	1/ 29 6	27	29.8	1/1 88	85.5	79.2			
Water - water	1/ 25 0	29	32.3	1/2 56	85.6	71.2			
Water -salt soluti on	1/ 26 2	28	30.3	1/2 53	88.1	81.3			
Water - water	1/ 17 0	28	31	1/1 75	82.7	68.8			
Water -salt soluti on	1/ 18 0	29	31.6	1/1 88	86.2	80.1			

2.6.3 By varying salt water concentration:

Table 2.6.3 Observation table for By varying salt water concentration

combi	Shel	l side	9	Tube side			
nation							
		Inlet	Outlet	Flow	Inlet	Outlet	
	Fl	wate	water	rate	water	water	
	0	r	temper	(lps)	temp	temper	
	w	temp	ature(°		eratu	ature	
	ra	eratu	C)		re es	(°C)	
	te	re(°C			(°C)	arch in	
	(lp)					
	s)						
Water	1/	28	30.2	1/1	81.6	78.2	
-salt	20			78			
soluti	0						
on 5:1							
Water	1/	28	30.4	1/3	86.3	83.3	
-salt	25			03			
soluti	6						
on 5:1							
Water	1/	29	31.1	1/2	84.6	81.4	
-salt	19			03			
soluti	3						
on 5:1							
Water	1/	28	29.8	1/1	87.7	80.2	
-salt	19			87			
soluti	3						
on							

20:1						
Water -salt soluti on 20:1	1/ 16 0	27	28.8	1/2 26	82.1	75.8
Water -salt soluti on 20:1	1/ 14 6	29	30.3	1/2 17	83.7	77.1

3.Results and Discussion

WATER-WATER combination:

Initial water temperature = $31^{\circ}C$ For tube water, time required to fill 1 liter bottle $t_{tube} = 171 \ sec$ For shell water, time required to fill 1 liter bottle $t_{shell} = 107 \ sec$ $Q = A \times V$ For tube water, $(1 \times [10]^{(-3)})/171$ $= \pi/4 \times (5.5/1000)^2 \times V_{tube}$ $V_{tube} = 0.246 \ m/s$ For shell water, $(1 \times [10]^{(-3)})/107$ $= \pi/4 \times (5.5/1000)^2 \times V_{shell}$ $V_{shell} = 0.393 \ m/s$ Water temperatures $t_{inlet} = 86.8^{\circ}C \& t_{outlet} = 76^{\circ}C$

WATER-SALT SOLUTION combination:

Initial water temperature = 29° C For tube water, time required to fill 1.2 liter bottle $t_{tube} = 148 \ sec$ For shell water, time required to fill 1.2 liter bottle $t_{shell} = 202 \ sec$ $Q = A \times V$ For tube water, $(1.2 \times [10]^{-(-3)})/148$ $= \pi/4 \times (5.5/1000)^2 \times V_tube$ $V_{tube} = 0.3412 \ m/s$ For shell water, $(1.2 \times [10]^{-(-3)})/202$ $= \pi/4 \times (5.5/1000)^2 \times V_shell$ $V_{shell} = 0.250 \ m/s$ Water temperatures $t_{inlet} = 82.5^{\circ}C \ \& t_{outlet} = 78.7^{\circ}C$

Result :

Water - water combination

 $Q_{\text{Rejected}} = m \times C_p \times \Delta T$ $= \rho \times Q \times C_p \times (\Delta T)$

Taking ρ at 81°C = 970.97 kg/m³



$$= 370.97 \times \frac{1 \times 10^{-3}}{171} \times 4.187 \times (86.8 - 76)$$

= 256.7 Watt

Salt water - water combination

 $Q_{\text{Rejected}} = m \times C_p \times \Delta T$

 $= \rho \times Q \times C_p \times (\Delta T)$

Taking ρ at 80°C = 971.7 kg/m³

$$= 971.1 \times \frac{1.2 \times 10^{-3}}{202} \times 4.187 \times (82.5 - 78.7)$$
$$= 91.786 \text{ Watt}$$

The results obtained from the above observations are as follows:

5.3.1 Observation for 7:1 concentration for salt waterwater combination

Table 5.3.1 Result table for 7:1 concentration for saltwater-water combination

com bin atio n	She	ll side			Tube side					
	Fl o w ra te (l p s)	inlet wate r temp eratu re(°C)	Outle t wate r temp eratu re(°C)	velo city(m/s)	Fl o w ra te (l p s)	Inle t wat er tem per atur e (°C)	Outl et wat er tem per atur e (°C)	Velo city(m/s)	o w (w at t)	
Wat er- wat er	1 / 1 0 7	27	30	0.39 31.010	1 / 1 7 1	86.8	76	0.24 6	2 5 6. 7	
Wat er- salt solu tion	1 / 2 0 2	29	31.5	0.25	1 / 1 4 8	82.5	78.7	0.34 1	9 1. 7 8	
Wat er- wat er	1 / 1 1 0	28	31.2	0.38 3	1 / 1 7 5	88.9	(79 (8 ₅ 8 (0.24 1 0/ch	2 5 0. 3	
Wat er- salt solu tion	1 / 2 0 5	30	32.8	0.20 5	1 / 1 5 1	85.5	81.2	0.27 9	8 9. 4	
Wat er- wat er	1 / 1 0 6	29	32.1	0.39 8	1 / 1 6 8	85.6	74.1	0.25 1	2 6 1. 7	
Wat er- salt solu tion	1 / 1 9 8	30	33	0.21 3	1 / 1 4 5	81.2	76.6	0.29 0	8 4. 2	

5.3.2 By keeping tube side and shell side fluid flow rate constant:

Table	5.3.2	Result	table	for	By	keeping	tube	side
and shell	side fl	uid flov	v rate	con	stan	ıt		

com bin atio	She	ll side			Tub	e side			H ra t
n	Fl o w ra te (l p s)	inlet wate r temp eratu re(°C)	Outle t wate r temp eratu re(°C)	velo city(m/s)	Fl o w ra te (l p s)	Inle t wat er tem per atur e (°C)	Outl et wat er tem per atur e (°C)	Velo city(m/s)	fl o w (w at t)
Wat er- wat er	1 / 1 8 0	28	31.6	0.23	1 / 1 9 0	83.4	70	0.22 2	3 0 0. 8
Wat er- salt solu tion	1 / 2 9 6	27	29.8	0.21 5	1 / 1 8 8	85.5	79.2	0.22 4	9 6. 2
Wat er- wat er	1 / 2 5 0	29	32.3	0.16 8	1 / 2 5 6	85.6	71.2	0.16 4	3 5 0. 3
Wat er- salt solu tion	1 / 2 6 2	28	30.3	0.16	1 / 2 5 3	88.1	81.3	0.16 8	9 5. 3
Wat er- wat er	1 / 1 7 0	28	31	0.24 8	1 / 1 7 5	82.7	68.8	0.24 1	3 6 0. 8
Wat er- salt solu tion	1 / 1 8 0	29	31.6	0.23 4 2 2	1 / 1 8 8	86.2	80.1	0.22 4	9 8. 3

5.3.3 By varying salt water concentration:

Table 5.3.3 Result table for By varying salt water concentration

60	Sho	ll cido			Tuk	o cido			ц
	Sile	II Slue			Tut	e siue			11
mbi									r
nati									at
on									fl
	Fl	inlet	Outle	velo	Fl	Inle	Out	Velo	0
	0	wate	t	city(0	t	let	city(w
	w	r	wate	m/s	w	wat	wat	m/s	(
	r	temp	r) ́	r	er	er) Í	w
	at	eratu	temp	-	at	tem	tem	-	at
	е	reſ°C	eratu		е	per	per		t)
	(l)	re(°C		(1	atur	atur		ŕ
	Ď	,	ì		Ď	е	е		
	s)		,		s)	(°C)	(°C)		
	-,				-,	(-)	()		
Wat	1	28	30.2	0.21	1	81.	78.	0.23	6
er-	/	-		0	/	6	2	7	0.
salt	2			-	1	-	_	-	2
colu	0				7				-
solu	0				/				



tion 5:1	0				8				
Wat er- salt solu tion 5:1	1 / 2 5 6	28	30.4	0.16 8	1 / 3 0 3	86. 3	83. 3	0.13 9	4 9. 1
Wat er- salt solu tion 5:1	1 / 1 9 3	29	31.1	0.21 8	1 / 2 0 3	84. 6	81. 4	0.20 7	6 8. 9
Wat er- salt solu tion 20: 1	1 / 1 9 3	28	29.8	0.21 8	1 / 1 8 7	87. 7	80. 2	0.22 5	9 5. 7
Wat er- salt solu tion 20: 1	1 / 1 6 0	27	28.8	0.26	1 / 2 6	82. 1	75. 8	0.18 6	1 0 0. 2
Wat er- salt solu tion 20: 1	1 / 1 4 6	29	30.3	0.28 9	1 / 2 1 7	83. 7	77. 1	0.19	1 5 0. 6

The observations are the result of simplification of model and uncertainties of numerical calculation. Also, inability of getting constant flow rate in both solutions might have impacted the results since flow rate of water-water combination is greater than flow rate of water-salt solution combination in observation. Also, Specific heat of salt solution varies according to solution concentration. Density of salt solution is less than water. Difference in turbulence of water and salt solution also has impact on results.

The results for heat flow rate of water-water solution and water-salt solution are 256.7and 91.78 watt respectively. Heat flow rate for water-salt solution is less than the water-water combination.

4.Conclusions

1.As seen in the calculations we can conclude that when we change the shell side fluid from water to salt water heat rejection rate decreases.

2.Thermal conductivity, density, specific heat etc. of salt solution is less than the properties of water. So, the heat transfer rate in case of salt solution in shell is less as compared to that of water in shell.

3. Turbulence in water is higher than salt solution. This has an impact on heat flow rate difference between water-water and water - salt solution combination.

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